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Structure and Dynamics of Combustion Waves in Premixed Gases

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Lecture VII Flame kernels and quasi-isobaric ignition

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Lecture 7: Flame kernels and quasi-isobaric ignition

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- 7-2. Zeldovich critical radius
- 7-3. Critical radius near the flammability limits
- 7-4. Dynamics of slowly expanding flames
- 7-5. Quasi-steady dynamic of thin flames Semi-phenomenological model Opened-tip Bunsen flames

VII-I) Introduction

Flammability limits X Critical conditions of ignition

Some hydrocarbon lean mixtures that are flammable cannot be ignited quasi-isobarically Some hydrocarbon rich mixtures that are non-flammable can sustain curved flames

Limits for upstream propagation \neq downstream propagation



Ignition in turbulent flows

Princeton experiments (2014) Wu & al.

Turbulence facilitates ignition of hydrocarbon lean mixtures Turbulence may suppress ignition of hydrocarbon rich mixtures

VII-2) Zeldovich critical radius

Flame kernel for a flame far from the flammability limits

Unstable steady spherical solution for the one-step model of adiabatic flames



Zeldovich

$$\begin{split} \theta &\equiv (T - T_u)/(T_b - T_u) \qquad \psi \equiv Y/Y_u \qquad \tau_{rb} \equiv \tau_r(T_b) \qquad c_p(T_b - T_u) = q_R Y_u \\ \Delta \theta &= \frac{1}{R^2} \frac{d}{dR} \left(R^2 \frac{d\theta}{dR} \right) \qquad \Delta \psi = \frac{1}{R^2} \frac{d}{dR} \left(R^2 \frac{d\psi}{dR} \right) \\ &\text{No flow} \\ -D_T \frac{1}{R^2} \frac{d}{dR} \left(R^2 \frac{d\theta}{dR} \right) = D \frac{1}{R^2} \frac{d}{dR} \left(R^2 \frac{d\psi}{dR} \right) = \frac{\psi}{\tau_{rb}} e^{-\beta(1-\theta)} \\ R &\leq R_f: \quad \theta = \theta_f, \quad \psi = 0; \qquad R \to \infty: \quad \theta = 0, \quad \psi = 1 \\ &\text{Flame temperature} \\ &\text{Le} \neq 1 \Rightarrow T_f \neq T_b \\ D_T \frac{d}{dR} \left(R^2 \frac{d\theta}{dR} \right) + D \frac{d}{dR} \left(R^2 \frac{d\psi}{dR} \right) = 0 \\ &\text{double integration from } R = 0 \text{ to } R = \infty \end{split}$$

$$D_T \theta = D(1 - \psi) \quad \Rightarrow \quad \theta_f = 1/\text{Le}$$



onservation energy)

$$Le \equiv D_T / D$$
$$Le < 1 \Rightarrow T_f > T_b$$
$$Le > 1 \Rightarrow T_f < T_b$$

Unstable **steady spherical solution** for the one-step model of adiabatic flames P.Clavin VII

> burnt gas

$$\theta \equiv (T - T_u)/(T_b - T_u) \qquad \psi \equiv Y/Y_u \qquad \tau_{rb} \equiv \tau_r(T_b) \qquad c_p(T_b - T_u) = q_R Y_u$$
$$-D_T \frac{1}{R^2} \frac{\mathrm{d}}{\mathrm{d}R} \left(R^2 \frac{\mathrm{d}\theta}{\mathrm{d}R} \right) = D \frac{1}{R^2} \frac{\mathrm{d}}{\mathrm{d}R} \left(R^2 \frac{\mathrm{d}\psi}{\mathrm{d}R} \right) = \frac{\psi}{\tau_{rb}} \mathrm{e}^{-\beta(1-\theta)}$$
$$R \leqslant R_f: \quad \theta = \theta_f, \quad \psi = 0; \qquad \qquad R \to \infty: \quad \theta = 0, \quad \psi = 1$$

Asymptotic analysis $\beta \gg 1$

temperature concentration reaction rate **Thin reaction zone** $\beta \to \infty$ thickness \ll flame radius R_f $x \equiv R - R_f, \quad |x| \ll R_f : -D_T \frac{\mathrm{d}^2 \theta}{\mathrm{d}x^2} = D \frac{\mathrm{d}^2 \psi}{\mathrm{d}x^2} = \frac{\psi}{\tau_{rb}} \mathrm{e}^{-\beta(1-\theta)}$ $\eta \equiv \beta(x/R_f) = O(1), \qquad \eta \in [-\infty, +\infty] \qquad \psi \equiv \operatorname{Le}(\theta_f - \theta) \qquad \psi e^{-\beta(1-\theta)} = e^{\beta(\theta_f - 1)} (\operatorname{Le}/\beta) \Theta e^{-\Theta}$
$$\begin{split} \Theta &\equiv \beta(\theta_f - \theta) = O(1) \qquad \Theta \in [0, \infty] \\ & \text{Inner variables} \qquad \qquad \frac{\mathrm{d}^2 \Theta}{\mathrm{d}\eta^2} = \frac{R_f^2}{D_T} \frac{\mathrm{e}^{\beta(\theta_f - 1)}}{\beta^2 \tau_{rb}} \mathrm{Le} \, \Theta \mathrm{e}^{-\Theta} \end{split}$$
Inner variables $\times \frac{\mathrm{d}\Theta}{\mathrm{d}\eta} + \int_{0}^{\Theta} \mathrm{d}\Theta \quad \Rightarrow \quad \beta \to \infty: \quad -\lim_{\Theta \to \infty} D_T \frac{\mathrm{d}\theta}{\mathrm{d}R} = \mathrm{e}^{\beta(\theta_f - 1)/2} \sqrt{2 \,\mathrm{Le} \frac{D_T}{\beta^2 \tau_{rb}}}$

External zones

$$\frac{R}{\mathrm{d}R} \left(R^2 \frac{\mathrm{d}\theta}{\mathrm{d}R}\right) = 0 \qquad R^2 \frac{\mathrm{d}\theta}{\mathrm{d}R} = \operatorname{cst.} \quad R = R_f: \quad \theta = \frac{1}{\mathrm{Le}} \frac{R_f}{R}, \quad R = R_f: \quad D_T \frac{\mathrm{d}\theta}{\mathrm{d}R} = -\frac{1}{\mathrm{Le}} \frac{D_T}{R_f} \qquad R < R_f: \quad \theta = \theta_f$$

Radius of the kernel

$$\begin{array}{l} \text{matching} \Rightarrow \frac{1}{\text{Le}} \frac{D_T}{R_f} = e^{\frac{\beta}{2} \left(\frac{1}{\text{Le}} - 1\right)} \sqrt{\text{Le} \frac{D_T}{\tau_b}} \Leftrightarrow \boxed{\frac{R_f}{d_L} = \text{Le}^{-3/2} e^{\frac{\beta}{2} \left(1 - \frac{1}{\text{Le}}\right)}}, \\
\begin{array}{l} \text{Le} < 1: \ R_f \ll d_L & \text{Le} > 1: \ R_f \gg d_L \\ \end{array} \qquad \begin{array}{l} \tau_b \equiv \beta^2 \tau_{rb}/2, \quad d_L \equiv \sqrt{D_T \tau_b} \\
\end{array}$$

Instability ? (adiabatic condition)

$$\theta = \theta_f R_f/R$$
 $\theta_f = 1/\text{Le} = \text{cst.}$ preheated zone at rest
 $\mathrm{d}\theta/\mathrm{d}R|_{R=R_f} = -\theta_f/R_f$

heat flux towards the preheated zone

convection should be added to restore equilibrium

Quasi-isobaric ignition as a nucleation problem

Le < 1 : $\overline{R}_f \ll d_L$ Le > 1 : $\overline{R}_f \gg d_L$

Lean hydrocarbon mixtures Le > 1 are difficult to ignite $(R_f > d_L)$

$$D_{C_nH_m} < D_{O_2} \approx D_T$$
, Le $\approx D_{O_2}/D_{C_nH_m} > 1$

Stability analyses

Stabilization in the presence of heat loss for Le < 1 (Buckmaster, Joulin, Ronney 1990) Flame balls in micro-gravity experiments (Ronney 1985-2004) (Deshaies Joulin 1984) lean hydrogen mixtures, diameter = 2 - 15 mm Extension of the Zeldovich analysis to a constant energy source



VII -3) Critical radius near the flammability limits (He Clavin 1993-94)

$$-D_{T}\frac{1}{R^{2}}\frac{\mathrm{d}}{\mathrm{d}R}\left(R^{2}\frac{\mathrm{d}\theta}{\mathrm{d}R}\right) = D\frac{1}{R^{2}}\frac{\mathrm{d}}{\mathrm{d}R}\left(R^{2}\frac{\mathrm{d}\psi}{\mathrm{d}R}\right) = \dot{W}$$

$$R \leqslant R_{f}: \quad \theta = \theta_{f}, \quad \psi = 0; \qquad R \to \infty: \quad \theta = 0, \quad \psi = 1$$

$$\begin{cases} T > T^{*}: \quad \dot{W} = \frac{\rho_{b}}{\rho_{u}}\frac{\psi^{2}}{\tau_{rb}}\left[\mathrm{e}^{-\beta(1-\theta)} - \mathrm{e}^{-\varepsilon}\right] \\ T < T^{*}: \quad \dot{W} = 0 \end{cases}$$

$$\frac{1}{\tau_{rb}} \equiv \frac{1}{\tau^{*}}\mathrm{e}^{\frac{E}{k_{B}}\left(\frac{1}{T^{*}} - \frac{1}{T_{b}}\right)} = \frac{B_{4f}}{B_{5f}}B_{1f}\mathrm{e}^{-\frac{E}{k_{B}T_{b}}}c^{*}_{\mathrm{O}_{2}u}$$

 $\varepsilon \equiv \beta \frac{(T_b - T^*)}{(T_b - T_u)} > 0 \quad \beta \equiv \frac{E}{k_B T_b} \left(1 - \frac{T_u}{T_b} \right) \gg 1 \quad \begin{cases} \varepsilon = O(1) : \text{ near to flammability limits } (\varepsilon = 0 : \text{ quenching } \dot{W} = 0) \\ \varepsilon \gg 1, \ e^{-\varepsilon} \approx 0 : \text{ far from flammability limits} \end{cases}$

Thin reaction zone $\beta \to \infty$ (non-dimensional form $\zeta = x/d_L$, d_L for $\varepsilon \gg 1$, Le = 1, 2nd reaction order)

$$-d^{2}\theta/d\zeta^{2} = \dot{w}(\theta,\psi), \quad (1/Le)d^{2}\psi/d\zeta^{2} = \dot{w}(\theta,\psi) \qquad \theta = \theta_{f}: \psi = 0$$
$$\frac{D_{T}}{d_{L}^{2}} = 4\frac{\rho_{b}}{\rho_{u}}\frac{1}{\beta^{3}\tau_{rb}}$$
$$\psi = Le(\theta_{f} - \theta)$$

$$\begin{cases} T > T^*: \quad \dot{\mathbf{w}} = (\beta^3/4) \operatorname{Le}^2 \mathrm{e}^{\beta(\theta_f - 1)} \left\{ (\theta_f - \theta)^2 \left[\mathrm{e}^{\beta(\theta - \theta_f)} - \mathrm{e}^{-\varepsilon - \beta(\theta_f - 1)} \right] \right\} & \qquad \theta^* \leqslant \theta < \theta_f \\ \theta^* \equiv \frac{T^* - T_u}{T_b - T_u} = 1 - \frac{\varepsilon}{\beta} \end{cases}$$

$$\times \frac{\mathrm{d}\theta}{\mathrm{d}\zeta} \Rightarrow \left(\frac{\mathrm{d}\theta}{\mathrm{d}\zeta}\right)^2 = \frac{\mathrm{Le}^2}{2} \mathrm{e}^{\beta(\theta_f - 1)} \int_{\theta^* = 1 - \varepsilon/\beta}^{\theta_f} \beta^3 (\theta_f - \theta)^2 \left\{ \mathrm{e}^{\beta(\theta - \theta_f)} - \mathrm{e}^{-\varepsilon - \beta(\theta_f - 1)} \right\} \mathrm{d}\theta \quad \text{at the exit of the reaction layer} \\ \left(\mathrm{entrance of the preheated zone} \right) \\ \theta^* = 1 - \varepsilon/\beta \\ \dot{w} = 0 \qquad 7$$

$$\left(\frac{\mathrm{d}\theta}{\mathrm{d}\zeta}\right)^2 = \frac{\mathrm{Le}^2}{2} \mathrm{e}^{\beta(\theta_f - 1)} \int_{\theta^* = 1 - \varepsilon/\beta}^{\theta_f} \beta^3(\theta_f - \theta)^2 \left\{ \mathrm{e}^{\beta(\theta - \theta_f)} - \mathrm{e}^{-\varepsilon - \beta(\theta_f - 1)} \right\} \mathrm{d}\theta \quad \text{at the exit of the reaction layer}$$
(entrance of the preheated zone)

$$\begin{split} \Theta &= \beta(\theta_f - \theta) \in [0, \Theta_f] \\ \mathrm{d}\theta &= -\beta \mathrm{d}\Theta \end{split} \qquad \Theta_f \equiv \beta \left(\frac{T_f - T^*}{T_b - T_u}\right) = \beta(\theta_f - \theta^*) = \varepsilon + \beta(\theta_f - 1) \geqslant 0 \\ \mathrm{measure of the distance from the flammability limit: } \Theta_f \in [0, \infty] \end{aligned}$$
$$(\mathrm{d}\theta/\mathrm{d}\zeta)^2 &= \mathrm{Le}^2 \mathrm{e}^{\beta(\theta_f - 1)} J(\Theta_f) \qquad J(\Theta_f) \equiv \frac{1}{2} \int_0^{\Theta_f} \Theta^2(\mathrm{e}^{-\Theta} - \mathrm{e}^{-\Theta_f}) \mathrm{d}\Theta \in [0, 1] \\ J(\Theta_f) &= 1 - \mathrm{e}^{-\Theta_f} \left(1 + \Theta_f + \frac{\Theta_f^2}{2!} + \frac{\Theta_f^3}{3!}\right) \quad \begin{cases} \Theta_f \gg 1: \quad J \approx 1 \\ 0 \leqslant \Theta_f \ll 1: \quad J \approx \Theta_f^4/(4!) \end{cases}$$

Preheated zone and matching

flame temperature of the spherical flame

$$R \ge R_f$$
: $\frac{\mathrm{d}\theta}{\mathrm{d}R} = -\theta_f \frac{R_f}{R^2}, \quad \theta_f = \frac{1}{\mathrm{Le}}$

$$\beta \to \infty : \frac{d_L}{R_f} = \text{Le}^2 e^{\frac{\beta}{2}(\frac{1}{\text{Le}} - 1)} \sqrt{J(\Theta_f)}$$

$$\begin{array}{c} T_f \to T^* \Rightarrow R_f/d_L \to \infty \\ \Theta_f \to 0 \end{array}$$

 T_b is determined by the composition of the mixture Y_{Ru} (mass fraction of the limiting component) T^* is determined by the chemical kinetics Y_{Ru}



Hydrogen rich mixtures

Hydrogen lean mixtures

Flammability limits X Critical conditions of ignition

Some hydrocarbon lean mixtures that are flammable cannot be ignited quasi-isobarically Some hydrocarbon rich mixtures that are non-flammable can sustain curved flames

Limits for upstream propagation \neq downstream propagation



Ignition in turbulent flows

Princeton experiments (2014) Wu & al.

Turbulence facilitates ignition of hydrocarbon lean mixtures

Turbulence may suppress ignition of hydrocarbon rich mixtures

simplest explanation:

Turbulent diffusion coefficients are all equal \Leftrightarrow 10Le > 1
Le = 1
Le = 1
Le < 1
Le turbulent

VII-4) Dynamics of slowly expanding flame kernels

Quasi-steady preheated zone of flame kernel ?

preheated zone in the reference frame attached to $R_f(t)$ $\dot{R}_f \equiv \frac{\mathrm{d}R_f}{\mathrm{d}t}$ $\frac{\partial\theta}{\partial t} - \dot{R}_f \frac{\partial\theta}{\partial R} - D_T \frac{1}{R^2} \frac{\partial}{\partial R} \left(R^2 \frac{\partial\theta}{\partial R} \right) = 0$ quasi-steady state ? $t_{relax} \equiv \frac{R^2}{D_T} \ll t_{evol} \equiv \frac{R_f}{\dot{R}_f} R \ll \sqrt{D_T t_{evol}}$, not valid at large distance

The evolution of spherical flame kernel cannot be quasi-steady at large distance

exact solution of the heat equation with a point energy source $\partial T/\partial t = D_T \Delta T$ point source, R = 0, t > 0: $\dot{Q}(t)$

$$\begin{split} \dot{Q} &= \mathrm{cst.} \qquad T(R,t) - T_u = \int_0^t \frac{\dot{Q}(t-\tau)}{\rho c_p} \frac{\exp(-R^2/4D_T\tau)}{(4\pi D_T\tau)^{3/2}} \mathrm{d}\tau \\ \dot{Q} &= \mathrm{cst.} \qquad X' \equiv R/\sqrt{4D_T\tau} \qquad \mathrm{d}X' = -2D_T R \frac{\mathrm{d}\tau}{(4D_T\tau)^{3/2}} \\ T - T_u &= \frac{1}{4\pi D_T} \frac{\dot{Q}}{\rho c_p} \frac{1}{R} \frac{2}{\sqrt{\pi}} \int_{R/\sqrt{4D_Tt}}^{\infty} \mathrm{d}X' \mathrm{e}^{-X'^2} \end{split}$$

relax time toward $(T - T_u) \propto 1/R$ increases with R like R^2/D_T $R^2/(4D_T t) \to 0$ For Le < 1 and near to the Zeldovich radius the slow evolution of flame kernels is governed by the diffusion at large distance

$$\tau \equiv t/t_{ref} \qquad \sqrt{t_{ref}} \equiv \frac{\beta(1 - \mathrm{Le}^{1/2})}{\mathrm{Le}} \frac{R_{fZ}}{(4\pi D_T)^{1/2}} \qquad \mathbf{r}_f \equiv R_f/R_{fZ}$$

Joulin's equation (Joulin 1985)

$$\frac{\beta}{2} \left(\theta_f - \frac{1}{\text{Le}} \right) = -\int_0^\tau \frac{d\tau'}{\tau'^{1/2}} \dot{\mathbf{r}}_f(\tau - \tau')$$
$$\frac{1}{\mathbf{r}_f} = \exp\left[-\int_0^\tau \frac{d\tau'}{\tau'^{1/2}} \dot{\mathbf{r}}_f(\tau - \tau') \right]$$



The structure and the dynamics of flame kernels \neq planar flames even for $R_f \gg d_L \ (\theta \approx \theta_f/R)$

Extension to a short pulse of an energy source (Joulin 1985)

Extension to the proximity of flammability limits + heat loss (Clavin 2015)

Dynamical quenching of flame kernels in **nonflammable mixtures** for Le < 1 (Clavin 2016)

$$\frac{1}{\sqrt{\mathbf{r}_f}} + H_b \mathbf{r}_f^2 = 1 - I(\tau) \quad \text{where} \quad I(\tau) \equiv \int_0^\tau \frac{\mathrm{d}\tau'}{\tau'^{1/2}} \dot{\mathbf{r}}_f(\tau - \tau')$$

Self-extinguished flames in micro-gravity experiments of lean methane-air mixtures (Ronney 1985-1990)



P.Clavin VII VII-5) Quasi-steady dynamics of thin flames ?

thin flames: flame thickness $(\approx D_T/\dot{R}_f) \ll R_f$ quasi-steady preheated zone $(R > R_f)$ evolution time \gg diffusion time on the flame thickness $x \equiv (R - R_f) \qquad \overbrace{\partial t}^{\partial \theta} - \begin{bmatrix} \dot{R}_f + 2 P_f \\ \dot{R}_f \end{bmatrix} \frac{\mathrm{d}\theta}{\mathrm{d}x} - D_T \frac{\mathrm{d}^2 \theta}{\mathrm{d}x^2} = 0 \qquad \frac{\dot{R}_f}{R_f} \ll \frac{D_T}{(D_T / \dot{R}_f)^2} \Leftrightarrow \qquad R_f \dot{R}_f \gg D_T$ moving frame $\Delta \theta \swarrow$ also negligible ! Quasi-steady state approx valid only when $\frac{R_f - U_L}{U_L} \ll 1, d \approx d_L, \frac{R_f}{d_L} \gg 1,$ Semi-phenomenological model Le=1.8, $\beta = 12.8$ $-\left[\dot{R}_{f}+2\frac{D_{T}}{R}\right]\frac{\mathrm{d}\theta}{\mathrm{d}x}-D_{T}\frac{\mathrm{d}^{2}\theta}{\mathrm{d}x^{2}}=0 + \text{asymptotic analysis } \beta \to \infty$ $-\left[\dot{R}_{f}+2\frac{D}{R}\right]\frac{\mathrm{d}\psi}{\mathrm{d}x}-D\frac{\mathrm{d}^{2}\psi}{\mathrm{d}x^{2}}=0 + \text{thin reaction zone } \Rightarrow F(\dot{R}_{f},R_{f})=0$ 1 Qs = 0 2 Qs = 1.5 3 Qs = 2 4 Qs = 3 5 Qs = 5 numerical results for a constant heat source extension of the Deshaies Joulin analysis (1983) by He (2000) numerical results of He (2000) extended to $R_f \dot{R}_f \approx D_T$! qualitative agreements with the experiments by Kelley et al. (2009)Figure 4. Variation of the flame velocity obtained from equation (12) with different values of the Steady converging flames. Opened-tip Bunsen flames Le < 1 Frankel Sivashinsky (1984) rich propane-air flame $U_{f} = -\dot{R}_{f} > 0 \qquad d_{L}/\dot{R}_{f} = O(1/\beta) \qquad \left(\frac{U_{f}}{U_{L}}\right) \ln\left(\frac{U_{f}}{U_{L}}\right) \stackrel{\text{Le} < 1}{=} -\left(\frac{1}{\text{Le}} - 1\right)\beta\frac{d_{L}}{R_{f}} \qquad \left(\frac{U_{f}}{U_{L}}\right) \ln\left(\frac{U_{f}}{U_{L}}\right) \stackrel{\text{Le} < 1}{=} -\left(\frac{1}{(\text{Le}^{-1} - 1)\beta d_{L}/R_{f}}\right) \stackrel{\text{Le} < 1}{=} -\left(\frac{1}{(\text{Le}^{-1} - 1)\beta d_{L}/R_{f}}\right)$ $\swarrow U_f/U_L$ no solution below a minimum radius 13 heavy hydrocarbon rich flame Almarcha Quinard (2015)